

Computational Analysis of pollutant production in the combustion



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Dedications

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Abstract

This research work relates to the numerical techniques for assisting to decrease formation of Soot formation present in emitted runoff streams carbon can be detached, and soot emissions can be decreased to very small levels. Further, the technique of this paper is useful to remove soot particles in IC combustion engines exhaust streams continuously. The given model assists to decrease in pollutants formation, which contains selective reducing agents. Initially, reduced selectively in high-grade fuels such as diesel surrounding to form the carbon-rich composition products. Results are obtained by implementing Moss-Brooks model results in ANSYS Fluent by comparing its results with experimental data from literature, through predicting different mechanism for the physical absorption coefficients of the soot. This paper comprehensively compiles the different models published for pollutants of combustion engines running on the road. Pollutants coming out of roads are broadly classified into two major groups unburnt hydrocarbons(soot) and non-stoichiometric oxides. Automobiles running on the road emit huge quantity of harmful pollutants into the atmosphere, among which NO_x, SO_x and a considerable amount of hydrocarbon soot. Simulation can be a relatively simple and effective tool for the reduction in amount of NO_x, SO_x, and Carbon Soot expelled by automobiles running on the road. In order to remove the harmful components from flue gases coming out of combustion engines to create a clean environment for future generation, Automobiles manufacturing companies should need to develop energy-efficient engines that are at the same time benign to environment. This is difficult and costly to reduce production costs together with the maintaining the same competitiveness level. Simulation model is also used to predict mechanism of soot and pollutants formation. The procedure of formation of pollutants is considered under discussion with an emphasis on the structure of their molecules and stoichiometric calculations. CFD is an effective tool that can simulate chemical reactions of all relevant phenomena occurring during the combustion in automobile engines and can be used for effective design based on physical and chemical parameters calculations of combustion engine to reduce the amount of pollutants.

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Chapter 1

Introduction

1.1 Soot formation

A soot formation is a multifaceted process, that is the evolution of the matter in which different number of the molecules go through different chemical and physical reactions that take place in few milliseconds. It is still not evidently understood that how the soot particles and the predecessors are formed in spite of extensive and wide studies available in review [16,17,24,28]. The information related to chemistry of formation of soot remained unanswered and debatable, but here are few points that are summarized below[18]:

- The nucleation of the heavy molecules occurs and form particles.
- Formation of soot reduced by soot particles by oxidation of their molecules.
- Soot begins with some building blocks or precursors.
- Coagulation happens through reactive particle-particle collisions.
- Particle surface growth proceeds by the adsorption of gas-phase molecules.

Different references projected varied the processes of soot formation within which several of them are in common. These wide united procedures proceeded in 3 steps that are portrayed in the Fig. 2. Giant aromatic rings are fashioned primarily through the addition of molecules of sunshine HCs (acetylene) within scale of molecules. Primary the soot particles are speculated to be fashioned either by the growth of surface or natural action of those compounds that are aromatic and are quite large. Tree and Sven's son [25] given the 5 steps involved in the formation of soot as portrayed schematically in the Fig. 3. In which, ethyne and the molecules of PAH are concerned throughout formation of precursor once fuel transformation., growth of surface, nucleation, jointure and the agglomeration are thought of as afterward steps.

According to Tree and Sven's son [25] mechanism of formation of soot, the hydrocarbon fuel is decomposed into tiny HC separated radicals. Anon hydrocarbon radicals that are else for the growth of the unsaturated hydrocarbons. Also, the adequately sizable amount of the atoms of

carbon in their structure. a rise within concentration of aliphatic compound acetylene chiefly play role in the formation of the giant benzene rings.

The sootparticles are then formed due coagulation of the larger aromatic structures making primarily soot particle. These particles instantly coagulate, at the same time finding out molecules from a gas section for the growth of surface. 5 main steps in the formation of soot are in brief mentioned in the next sub-sections.

1.2 Soot formation precursors

Different types that are thought of as the start for the formation of soot and evolution are cited by way of precursors. The beginning of soot may be a process through that the precursors are the results of combustion of fuel to create particles of soot. Beginning is poorly understood as a result of the emergent soot particles is extraordinarily little about one nm in the diameter. Creating experimental researches terribly tough [18]. Among them, alkyne has received more attention [30]. Alkyne is known by Glassman [24] and then afterward established by Howard and Richter [18] as a reallyvital precursor for the formation of soot in the combustion of diesel, presumably as a result of the primary aromatic rings that are fashioned by additions of C2 and C3 [31].

In 1990s, Frenklach and Wang [32] projected that acetylenes addition cause the creation of initial benzene rings. Because of restricted creation of some of the intermediate molecules through alkyne and complexness of investigational studies, the molecules of PAHs rather than acetylene are considered as precursor of soot in the combustion of diesel[33,34]. Formation of PAH and its growth seem to rely chiefly on the kind of fuel a number of reaction arrangements that represents the creation of 1st aromatic rings are givenin another place [26].

1.3. Nucleation

Nucleation is the subsequent step that is origination of the particles from serious molecules of PAH by forming links with each other and become a forming soot.

1.4. Mass growth

Growth of soot surface is that the overall process through that soot particles in plenty grow through the accumulation of gas species like alkynes and PAH molecules or radicals. There is no clear difference between top of nucleation and alsostarting of the growth of surface, and truly the 2 processes are synchronic.

1.5. Coagulation

Soot is mostly formed of the circular particles that are grouped together to form different shapes and arrangements like chain as given in Fig. 1a. The process of coalescence means the combination of smaller molecules to form huge particle during different processes like growth of particle and nucleation as in Figs. 2 and 3. [17,25].

1.6. Oxidation process

Different components that help in oxidation are O_2 , O in fuel-rich environments while H_2O , CO_2 , NO , N_2O , and NO are potential oxidants of fuel lean environments. The process of oxidation take place all the time in precise stage in contrast to growth of soot surface [19]. The results of different processes by changing the particles of solid soot to gaseous form as CO and CO_2 is known as soot reaction. The rate of oxidation is affected by the area of particles. The mass of carbon that is accumulated in soot particles is decreased by the reaction taking place on the surface of soot [17]. Many models of chemical reactions in which oxidants apart from oxygen are involved are given somewhere else [19,40]. A comprehensive literature for the basics of formation of soot procedure is away from the scope of the literature [16,17,24, 28].

1.7 Nox and SOx Formation

Other major issues in combustion of cars the production of pollution from various sources. Air pollution will take numerous forms. A number of the various sorts of air pollutants embody particulate emissions such as coal ash, partly burned coal particles, and the like, sulfur compounds like SO_2 and SO_3 (sometimes collectively observed as “SO”), ozone, carbon compound emissions, volatile organic compound emissions, and emissions of atomic number 7 oxides (commonly observed jointly as “NOx ‘). Combustion effluents and waste merchandise from specific sorts of sources have well-tried to be major contributors to damaging pollution once the effluents are discharged into the atmosphere unless these waste products are treated before unleash into the atmosphere, serious air pollution and pollution issues are encountered. It will be appreciated that top concentrations of air pollutants have serious harmful impacts on the health and general welfare of society. Pollution is known to worsen sure medical conditions (such as heart and respiratory organ issues) and is thought to cause problems within the surroundings, starting from corrosion to acid precipitation.

One of the foremost common elements found in contaminated air is gas (“NO₂”) that is thought to be toxic. Gas that is brown in color undergoes a series of reactions, well-known usually as “photochemical smog formation,” within the presence of sunlight and mobile hydrocarbons. These reactions result in a marked decline in overall air quality. While NO₂ is made from a good type of pollution sources, its primary supply is from gas (“NO”) discharged into the air. NO is often shaped during combustion processes, as well as burning engines in cars and different similar installations. There are 2 primary mechanisms for the formation of atomic number 7 oxides within the combustion processes. Within the warmth parts of flame, atmospheric oxygen will react with molecular atomic number 7 (“N₂) to form NO by the warmth “thermal fixation” mechanism. In addition, fuels that contain massive amounts of nitrogen with chemicals certain among the fuel structure may manufacture important nitrogen emissions as a result of the oxidation of the fuel atomic number 7 throughout the burning method. This supply of nitrogen emission (often termed “fuel NO_x) is that the predominant supply of nitrogen with the combustion of petrol and different fossil fuels. Since NO is that the solely compound of atomic number 7 that is stable at the high temperatures encountered in these varieties of combustion processes, NO is that the predominant atomic number 7 emission product. At traditional part temperatures, however, the equilibrium between NO and NO₂ favors NO₂. Hence, NO shaped by combustion is mostly discharged into the atmosphere as NO, and solely later regenerate to NO₂. So, as to manage NO₂ emissions; therefore, it’s necessary to eliminate NO before it enters the atmosphere.

An improved method of understanding soot formation created it attainable for formulating the scientific models that help in predicting the concentration and mass of the soot within processes of emissions, and help in validating the projected mechanisms, and successively smart models that are useful in higher understanding the characteristics of soot and the methods of formation. Important advancements are created on mechanisms of the formation of soot within last twenty years [16–19]. Though, it seems that still there is a niche between present models of soot and the actual processes for formation of soot. The gap get even larger once it involves the formation of soot from the burning of aerated energies because of variable compositions and numerous sorts of feedstock[20–22].

1.8 Mechanism of soot determination

Final concentration of soot is determined through different mechanism steps such as initiation, coagulation, surface growth of nanoparticles and the oxidation. Although acceptable results are obtained on laminar diffusion flames but phenomenon becomes too much complicated when turbulent chemistry is involved in diesel engines, as the soot prediction models are applied to simple straight-chain hydrocarbons.

1.9. Structure and composition of soot

For improved understanding of different mechanisms of the soot formation created within literature, it is worthy for concisely assessment the chemistry of soot. Soot could be in the form of a solid material which consists of about eight elements of the carbon along with one half of the nitrogen the chemical element (density of soot is 1.84701 g/cm^3 [23] and is also reported by different authors that fall close to such value. The soot is generally fashioned because of result of the combustion of the fuel in the engines with its different features don't seem the purposes of the fuel and different in operation environments [24]. The soot turns out to be a component of black carbon once gift inadequately massive size of particle and amount in the depleted gases. The soot that is nucleating from vapor part to the solid introduce the fuel-rich sections at the temperatures at increased value [13,14]. Hydrocarbons or different accessible molecules might get condensed or get absorption by the soot looking on the neighboring environments [25].

A recently fashioned particle of soot at first has best H content, and also the Carbon/Hydrogen magnitude relation is low collectively. Though, as the soot develops, the portion of carbon will increase. Small quantities of metal, calcium, phosphorus, silicon, iron, and metal are usually distinguished in the soot emitted from the diesel engine [13,14,26, 27].

Soot is usually found in different type of the clusters of sub-micron size [122]. As Fig. 1a could be a typical image soot of diesel taken with SEM(Scanning electron Microscopy) that show the agglomerates are formed of the assemblies of many tiny piece units in the circular or nearly spherical form [17]. The analysis through is XRD, is demonstrated in the Fig. 1b [28], which specifies the atomic groups of carbon of the chief particle of soot that are arranged in the form of polygon face-centered arrangements, ordinarily mentioned in the form of platelets. The platelets are organized in the form of layers to make crystallites, and commonly, there are sometimes 2 to 5 platelets in each crystal [28].

When examined underneath high-resolution transmission microscopy (HRTEM), 2 different elements of the main diesel particle of soot may be recognized: associate outer most boundary shell and the internal core, as illustrated in Figure 1c [29]. The living substance model, as discussed on top that is applied to the valance shell. Although, the internal central core consist of small cluster with acircularnuclei encircled by the carbon net-works having a twisting structure. It shows that outer shell, that consists of crystals of graphite, that is of a firm structure, whereas the inner core is with chemicals that are structurally less stable thanks to the physical science that is structure of instability. Sequence of the crystallites preparation that contain the inner or valance shells. The small particles in the composed soot (with totally different sizes ascertained underneath analysis of HRTEM).

In short, formation of the soot that is the alteration of molecules of fuel of HC into chemical element agglomerates is associate tremendously sophisticated method. It is the form of the gaseous-solid physical change wherever the solid part displays no distinctive physical and the chemical structures, and therefore conversion happens through varied chemical change and the physical collaboration phases. Variety of methods for the modeling of soot exist. However, there is trade-off among the potential of prediction of the small print of soot formation and process time. There is another major concern in modeling of soot production that the complexness of coinciding chemical and the physical processes, like precursor development from gas part chemistry, that is particle beginning, particle growth, nucleation, natural action and oxidation of particle that are exhausting to explain in a very sequence of the scientific formula. So, the basic models of soot that may turn out additional realistic ends up in the reduced process time are extremely chosen for different engine style and the emission management.

1.10 Damaging impacts

The soot unburnt carbonaceous material emission is real fact from all IC engines process due to high-temperature conditions. Hence, a forceful reduction in the emissions is obligatory, strict in a deeper understanding within the formation method that remains associate degree open problem in combustion chemistry analysis. In the recent years, ways for reduction in soot emissions relied primarily on correlations, expertise, and trial-and-error tries.

The conventional burning of natural gas has some drawbacks. For example, the only products of methane combustion should be carbon dioxide and water-based on the overall reaction. However, as a result of nitrogen oxide, i.e., NO₂ and NO, are also produced. The production of

NO_x is because of traditional burners operating at a temperature as high as 2000 K. The produced oxides are environmental pollutants causing the concerns. Furthermore, the incomplete conversion of methane in traditional combustion will result in the release of unconverted methane into the environment. The homogenous combustion of methane can only happen in a certain range of the flammability limits (5 to 16 % by volume of methane in the air). It can be considered that methane cannot be combusted with conventional combustion. These drawbacks have limited the use of conventional natural gas combustors. For example, the careful adjustment of the air and gas ratio for efficient burning; use of spark plugs for initiating combustion; the use of materials capable of sustaining high temperatures during the burning process, etc. In consideration of the environmental pollution use of the appropriate treatment of the effluent gas before release in the atmosphere is also required.

1.11 Soot modeling

Soot modeling will be enhanced as long because formation and the chemical reaction methods are understood evidently and consequently, a lot of accurate the norms are created. This literature commences by means of a quick explanation of the basics of development of soot and also reviews improvement of the soot modeling for the combustion of diesel. Since the first 1970, whereas giving a lot of stress on modeling the beat up the past twenty years that is then followed by fully different methods of modeling and the evaluation of these methods together with highpoints of the empirical and theoretical outcomes. It conjointly examines the specifications of models and its parameters and so the precision of the estimations for the presentation of model with respect to concentration of soot. The literature emphasis is principally on sensible models of soot for the combustion of vehicle of diesel established about the last twenty years.

1.12 CFD Simulations

CFD simulations are performed to analyze combustion process to predict soot and compare it with different soot model.

1.13 Simulation Setup

The physical process is done numerically by solving equations of the mathematical model in the computer system. This representation of equations is usually known as Numerical Simulation. This process has a tendency to produce results that are not achievable through other means. Numerical simulation usage is increasing day by day due to the increase in computer technology.

By centralizing a computing capacity in a single system to enhance the performance of that system is regarded as the best way to solve complex problems that can occur in the field of physics and engineering. The evolution in the computer market has made the researcher think to find the new ways of solving complex problems by using computer systems. This can save a lot of time and cost as well. Different simulation tools are available in the market to solve a different set of complex reactions and problems. Computational fluid dynamics is that branch of mechanical science that tends to analyze and solve problems which involve fluid flow systems in chemical reactors. This is way CFD software pack is known as the best designing tool for different areas of reaction engineering as well. This thesis is being done for the numerically simulated combustion process in the presence of a platinum group metal as a catalyst. Two-dimensional (2D) and three-dimensional (3D) CFD analysis are being done in this research thesis.

Methane combustion is performed under catalytic overheated wall surfaces. Rhodium is used as the catalyst surface for this process of combustion of methane. The chemical reactions which involve catalytic activity taking place on the surface of the catalyst require modeling of a cylindrical channel of heated catalyst wall which is used as a surface phenomenon for the catalytic combustion of methane inside the combustion chamber [31](Hickman and Schmidt 1993).

For two-dimensional (2D) modeling of the reactor, the cylindrical channel was designed with the 2D ax symmetric solver. The first step of simulation was to create a geometry model which represents the desired flow. Gambit software was used to create the geometry and mesh involving catalyst channel. Two-dimensional CFD code was used for this work. The reactor boundaries such as inlet, outlet, and walls were resolved on this software. The geometry consisted of catalytic walls through which the fuel-air mixture is passed on at high temperature.

1.14 Methane combustion

In methane, combustion soot grew up from small particles of carbon while in most common road applicable fuel such as diesel that contain large amount of aromatics gives large amount of soot. This paper gives the detail of different modeling techniques to predict soot formation involving turbulent chemistry during diesel combustion.

1.15 IC engine

During the process of burning (IC) diesel engines an unlimited quantity of the fuel is expended, and so that is the indication no of danger to the atmosphere in the terms of emissions of waste material. In the theoretical conditions, once the whole combustion of fuel is attained, entirely carbon dioxide and binary compound species are generated. Though, such type of conditions are not possible to realize because of engine transient in such operating conditions. In year 2013, twenty-five of the world emissions of carbon dioxide evolved from transportation segment(EnergyAgency,2015).Additionally, as a result of the IC engine operating conditions, many different types, like NO_x, HC, CO, and PM, are made. Comparative to the overall flue gases flow, a hundred forty-five belong to those species, of that roughly fiftieth are the species of NO_x (Khair and Majewski, 2006).

As an element of affinity towards the cleaner transport segment with the less effect on surroundings, amounts of emitted waste material emissions are controlled within the past decade (Klemeset al., 2012, and the lot of tight conditions are required by the policies of government each year. Examination to engines of sparks ignition, diesel engines can be defined by bigger energy transformation and the factor of safety Katrasnik, 2007).So as to stay the foremost used as vehicle powering supply on the market, additionally on meeting the upper potency standards, the IC engines potency should be perpetually enhanced Kozaracet al.,2014). Additionally to emission laws, another difficulty for IC engine exercise is the biofuels advancement within the transport segment (Niemisto et al., 2013). As an element of ecu-biofuels instruction (2003/30/EC) in year 2003, a smallest level of the used biofuel was imposed to all or any members of the states of EU.

1.16 Biodiesel

Biodiesel comes by the process of trans-esterification, not containing sulphur, destroys quickly, that is nontoxic. Additionally, to the optimization of performance of engine, NO productions may be decreased by introducing varied depleted recirculation of gas and the boosting systems of engine.

1.17Method of combustion

The method of combustion among IC diesel motor are often divided in 2 different parts: an overpowering premixed combustion taking place throughout the procedure of auto ignition, and

the combustion of mixing-controlled diffusion. Maximum of the gasified fuel is then combusted within regime of diffusion and thus the general engine potency is extremely dependent on spray method. Spray could be extremely transient and also turbulent point in time method, that is consisting of many different processes, like disintegration of fuel jet, collision and dribble atomization, AN evaporation method and air entrainment.

1.18 Approaches for modeling

Spray could be a multipurpose method, but interior combustion engines additionally employed in the removal of waste emissions (Baleta et al., 2016), and also the various experimental researches are also performed. Though, with progress of procedure power and the development of procedure Fluid Dynamic (CFD) tools, along with investigational analysis with analysis of CFD turned into common method. With this approach, associate understanding of the advanced and the temporary turbulent flows which are arduous to the capture by experimentation is considerably enhanced. For consistent use of tools of CFD, every used sub models ought to be antecedently validated. Finally, combination of the CFD tools with investigational analysis might end in a discount of general expenses and the examination length.

Different approaches are developed for procedure modeling of the turbulent spread polyphase flows, like separate Particle Model (DPM), Direct Numerical Simulation (DNS) for particles, the Leonhard Euler Eulerian (EE) model, and also the Euler-Lagrangian (EL) etc. (Martin Sommerfeld and Berend van Wachem, 2008).

1.19 Euler- Lagrangian technique

The EL method is that the mostly used technique for demonstrating the spray method. whereas it has many drawbacks like parallel calculation potency reduction, mesh dependency, the EL approach, high particle loading, is sufficiently correct and economical for the modeling diluted spray region, as revealed for the liquids by Faeth et al. (1995), likewise as for the solid particles. Presented literature on the usage of the biodiesel combinations as fuel in the compression-ignition engines usually provide information on reduction in particulate matter (PM), organic compound (HC) and emissions of monoxide as advantages, additionally as hyperbolic levels of Night emissions joined of most disadvantages of the biodiesel execution . Nevertheless, a vast awareness into the reported investigational results queries this growing tendency and examines its reasons. as an example, the complete review of literature examined variations in the fuel injection system and the combustion because of differences in the physical and also chemical

properties of the biodiesel, like lower heating worth, elastic modulus and also the viscosity, etc. It's equally (Sun et al., 2010) all over that, though the rise in production of carbon dioxide exists, that is not intrinsic to the biofuel itself, however, because of the usage of the biodiesel in unadapted diesel systems. The distinction in the properties of biodiesel developments the beginning of the inoculation method and will increase the temperatures for combustion, resulting in the increased Night emissions. In the actual experimental systems, it's typically onerous to make sure constant operational limitations once examination totally dissimilar fuels (e.g., the identical begin and also the finish of the injection). In such things, numerical simulations are often an excellent tool for the analysis and the evaluation of the performances of various fuels within same operating managements.

It is amongst this paper objectives for statistically investigating the NO_x waste material emissions once exploitation biodiesel mixture, as compared with the alike conditions with the normal fuel. Therefore, it's vital to know the process of thermochemistry behind NO_x formation. The nitrogen-containing emissions that are evolved from the processes of combustion are normally divided as prompt, thermal, and the fuel NO_x.

Even though elaborate kinetic procedures exist (Miller and expert, 1989), so as to get the model that is computationally economical, different interpretations have to be created. Chemical model interpretations, like omitting species with the light concentrations, other of removing the reaction methods with small effect on the Night production or idea of chemical equilibrium are a standard method for simplifying complicated chemical phenomena that are used in CFD. Less variety of the chemical equations permits for associate economical link along with turbulent reacting flow. Interaction of chemistry-turbulence was demonstrated by taking under consideration the fluctuations of temperature, desegregating the chemical process rates, and then applying the likelihood Density perform (PDF) method (Vujanovic et al., 2009).The Conferred arithmetic model that is for modeling Night emissions that has been enforced within CFD code fireplace.

1.20 Combustion species

Diesel is understood as supply of the emission types like PAHs that are polycyclic aromatic hydrocarbons, particulate (PM), significant metals, and (NO_x) the oxides [4,5]. Such species that are created from the combustion and located in the productions primarily within style of aerosols, and are known as dangerous for health [6,7]. Amongst the diesel emission parts, PM₅ has a heavy concern for the health of human and also thanks to their direct and the wide-ranging

influence that is on the organs of metastasis[4,5]. In ancient eras, the specialists of health-related PM10 (diameter 10 μm) with the long-lasting respiratory organ malady, carcinoma, influenza, asthma, and also the reason for enhanced mortality rate [117]. Though, present scientific research recommends that these associations be a lot of thoroughly joined with the fine particles that are (PM2.5) and also the very-fine particles that are (PM0.1) [118], as a result of the fine and the ultra-fine particles will simply get penetrated deep into lungs.

Metal oxides and noble metals have been widely used as combustion catalysts. Generally, noble metals have higher activity as compared to the metal oxides [119](Anderson, Stein, et al. 1961). The catalysts used in combustion process can either be supported or without support. Usually, catalysts with support are preferred because of the better utility of the precious catalyst spread over the support. It provides better yield, better activity, and uses less amount of catalyst giving the maximum surface area of the catalyst. The catalysts with support have better thermal stability. Another advantage of the support is that it can also play a role in the oxidation reaction. In oxidation reaction, the support may provide the storage capacity.

Generally, the ideal catalyst for the combustion should have following characteristics;

1. High Activity
2. Low ignition temperature
3. High thermal stability
4. Stable activity
5. Resistance to poison
6. Low price
7. Nontoxicity

It is not necessary that the catalyst should comprise of all above characteristic. However, the above qualities can be used to determine the quality of catalyst and can help in choosing the right catalyst for the desired application.

CHAPTER 2.

LITERATURE REVIEW

2.1 Literature Review

Models that are supported by phenomenological explanation have found wide use in the recent time. Phenomenological soot models that can be categorized as the semi-empirical models can be correlated by trial and error ascertained phenomena in an exceedingly method that's in line with the basic theory, however, isn't directly derivative of the speculation. Phenomenological models also use sub-models that are established to explain the various methods ascertained throughout the process of combustion. These sub-models will be by trial and error established from the observation or by victimizing basic physical and the chemical relations. The benefits of such phenomenological models are such that they're quite consistent and nonetheless not thus sophisticated. So, they're helpful, particularly once the precision of parameters of the model is low.

This software is well established for different types of reaction engineering. Combustion of fossil fuels has been known as the primary component for the energy sources. The importance of combustion process and its usage has been enhanced by the increase in demand for energy in the present era. But this process is also intimidated as the source for the emission of extensive pollution of the environment. The reason behind this pollution is the components that are emitted during this process, which causes a lot of damage to the environment. That is why these environmental pollutants are the major challenge in the development and planning departments of the energy sector. For achieving the requirement of environmental standards, it is necessary to come up with the efficient procedure which reduces such components emission and maximizes the efficiency of the combustion process. Catalytic combustion is known as the efficient process in order to eliminate such substances which are dangerous for the environment. The reason

behind it is because this process requires very low energy and still performs quiet, efficient conversion by removing these organic compounds. A lot of research has already been carried out in the past regarding CFD and methane combustion. This research is also done by keeping in mind whatever the previous work has been done and what results have been achieved. In this section of the thesis, we will discuss the previous researchers that have been carried out involving catalytic combustion and their analysis through different simulation-based software like Aspen Plus, Computational Fluid Dynamics (CFD), MATLAB, etc.

Methane combustion is a process which is used on a large scale for the production of heat and power for different industrial units. Catalytic combustion is regarded as the fast-exothermic reaction usually carried out in a fluid bed reactor. Different experimental researches have been done on this process historically, and by the innovation of computer technologies in the market, researchers have developed software's which can predict the results for such experimental results by simulating required input data. Computational Fluid Dynamics (CFD) is a latest emerging approach which is used to predict simulation-based results by incorporating required information in the software. CFD provides an internal visualization aid compared to other computer-based software's like Aspen Plus, MATLAB, etc. Veldsink [20](Veldsink, Versteeg, et al. 1995) studied the intrinsic kinetics of the methane oxidation on industrially available copper oxide with alumina support. He studied the kinetic rate of methane combustion taking place in the presence of a catalyst at temperatures ranging from 723k to 923k. Copper oxide was used on alumina support as a catalyst for the catalytic combustion process. This study was carried out in order to know the capabilities of this process for a membrane reactor. He concluded that this could be studied without limitations of heat and mass transfer in packed bed reactors. He also concluded that the catalyst used was quite efficient for such purpose as it long lasted and stable for high temperatures. He also derived rate equations and explained that there was no methane adsorption was found on a catalyst surface. Dangi and Abraham [21](Dangi and Abraham 1997) performed complete catalytic combustion of benzene and methyl tert-butyl ether. They obtain experimental parameters from pure component experiments and then put into their model for the prediction of the simulation. They concluded from their research that complete oxidation of benzene and methyl tert-butyl ether results in the production of carbon dioxide and water due to the complete destruction at a temperature ranging from 400-500 °C. They also discussed details of the adsorption of material on the catalyst surface at low temperature. Mars van krevelen model was

used for their model assumptions. Anthony G Dixon [24](Dixon and Nijemeisland 2001) performed his analysis on CFD by using fixed bed reactors. He explained through his research that Computational Fluid dynamics is the appropriate software which has the capability to give details of the temperature and flow fields. It can provide highly reliable information of the flow field regimes. Zakharov and Zolotarski [25](Zakharov, Zolotarskii et al. 2003) investigated about transfer of mass and flow of gas by using two stage system which involved catalytic oxidation occurring at nitric acid plants through the simulation of gauze pad honeycomb chemical reactor system. Rodrigo [26] used CFD software to predict the influencing parameters involving in the catalytic oxidation of vanillic acid. He performed the analysis within a trickle bed reactor to execute numerical simulations. Additionally, Deutschmann and Quiceno [27] reported the high temperature catalytic partial oxidation of methane over platinum gauze. Their work is evident that even for complex catalytic geometries, Computational Fluid Dynamic CFD is the best software available which has the capability to implement comprehensive homogeneous reaction scheme. Jiang and Khadilkar [28] reported the modelling of multiphase flow distribution by using simulation through CFD under steady and unsteady state conditions. The flow distribution was carried in the catalytic packed bed reactors under the influence of steady or unsteady state conditions. The reactors used were scale cylindrical or rectangular shaped packed bed reactors. The distribution of porosity in packed bed reactors were applied by using pseudo-randomly allotted cell section holdup distribution.

This unit gives the models of soot production through diesel combustion revealed primarily on the empirical and also semi-empirical methods. Many models that are applied in such classes take into account 2 competitive reactions that are formation of soot and the oxidization of soot, as a ballroom dance approach [40,47,49], both reactions are dependent on temperature, and that are delineated by physicist type expressions. The formation rate of soot production are directly depends upon the fuel pressure whereas they have no dependence on the fuel type. Each of that have an effect on the extent of soot accessible for the given mass of the soot created as it is explained in Section three. The oxidization expression comprises solely oxygen, due to different vital oxidization mechanisms like American state reactions.

Lindstedt made public steps for reaction for the growth and formation and of particles of soot [63]. Elaborate gas section chemistry and the basic steps of the growth surface, nucleation. The agglomeration of particle was combined within the model. The surface growth reactions and soot

nucleation are connected to the chemistry of gas section. Lindstedt paid abundant attention to the issues of modeling the growth of mass of soot. Lindstedt thought of the four models that are for the reactions of soot growth [42]. Additional details on present soot models are provided in Section four.2 that reports elaborate the mechanisms and also the phenomenological models of the soot yet.

After some years, Hiroyasu et al. [49] projected one among the foremost used models that are primarily supported by empirical formulas for the prediction of the formation and oxidization of the particles of soot. They noticed that their ballroom dance soot model was chiefly tormented by temperature, pressure and the equivalence quantitative relation, that is that the definite fuel foroxidizer quantitative relation and is regulated by the ratio of fuel to the oxidant ratio.

This model is includingthe formation of soot and oxidization rate, that includes the accessible mass of fuel and partial pressure of oxygen. Eq. (1) computes the primary order rate of internet formation of soot (dm_s/dt) employing a combination of therate of soot formation along with oxidization rate for the Hiroyasu's model. The rate equation of soot formation Eq. (2) according to arrhenius theory and is nearly the second order kinetics (1.8) of the pressure whereas its rate of formation could be a 0.5 order of the pressure.

$$\frac{dm_s}{dt} = \frac{dm_{sf}}{dt} - \frac{dm_{sc}}{dt} \quad (1)$$

$$\frac{dm_{sf}}{dt} = A_f m_{fg} P^{0.5} e^{(-E_{xf}/RT)} \quad (2)$$

$$\frac{dm_{sc}}{dt} = A_c m_s \frac{P_{O_2}}{P} P^{1.8} e^{(-E_{xc}/RT)} \quad (3)$$

where m_{fc} and m_{sf} is the mass of the oxidizes soot, and mass of soot formed respectively. E_{sc} and E_{sf} are the activation energies for oxidation of soot and formation of soot, respectively. By corresponding the predicted soot and the practically coming out soot within the exhaust A_c and A_f were determined. The Hiroyasu's model was very terribly useful for giving information on the majority transport and distribution of soot within the combustion environments having elevated temperature of typical diesel engines [51]. Furthermore, thanks to simple application into machine, Codes of computational fluid dynamic, the model along with its advancements have nonheritable spacious quality within the group involved in three-dimensional modeling simulation of diesel combustion [52]

The ballroom dancing approach of the Hiroyasu's model [49] is a simple empirical model having 2 steps to predict formation of soot. Hiroyasu's model soot formation formula is not dependent on the sort, structure, composition of the fuel. The chemical reaction expression includes solely element molecules within this model [53]. Hiroyasu's model is called as terribly sensible and easy, however it desires a lot of parameters for upgrading for the purpose of additional study [54– 56].

The soot model of Hiroyasu-Nagle and Strickland (HNS) has become popular because it was semi-empirical model of two-step for the formation of soot in the diesel combustion engine [47,61]. The soot formation rate and rate of oxidation were given another time in the Arrheniustype equation as follows:

$$\text{Rate of formation} = A_f P^{0.5} e^{-E_f/RT} \quad (4)$$

$$\text{Rate of oxidation} = X_{O_2} A_0 P^{1.8} e^{-E_0/RT} \quad (5)$$

As it was stated earlier that the formation of soot and reaction are terribly complicated, and it is impossible to precisely model a posh method solely with the simplified models. Not like empirical models and also semi-empirical models that extraordinarily modify the method for formation of soot, the elaborate model helps to describe the growth, formation, and reaction of soot with some close chemical change procedure. The extraordinarily increased demand of the calculating time of elaborate models of soot makes them impossible for the simulation of the combustion of ICE. Later, many of the investigations were conducted in an exceedingly real configuration like diesel engines use the procedure of coarse modeling schemes for their requirement of benefit of straightforward application and the low machine value. This part reviews the papers that are published that targeted on elaborate models and people with stress on the phenomenological ways.

With the new advances in engineering and the advances indifferent precise sub-models, it is currently attainable to get helpful assumptions and also conceptions of advanced systems. Consequently, the arithmetic simulation of the such advanced systems is taken into account in many fields. In the modeling of soot, many numerical approaches of simulations can be classified into 2 main modules that is flat CFD modeling and phenomenological models. In phenomenological models explain the new method of the formation of soot and reaction in the

terms of many international steps those are significantly beneficial for the combustion simulations.

The model of Fusco et al. [66] in 1994 planned a model for soot to beat different limitations of earlier models of soot for conditions of combustion of ICE. This model takes accounts for amount of the carbon atoms of main fundamental molecules within fuel that incorporates physical method of origination, surface growth, activity and reaction into phenomenological model of soot having eight different steps. The model is consist of 4 differential equations equalization among the rates of the particle range modification, soot radical precursors, acetylene and the volume fraction of soot. As like the previous preparations, expression of Arrhenius-type rateis the one that has been used for the most of

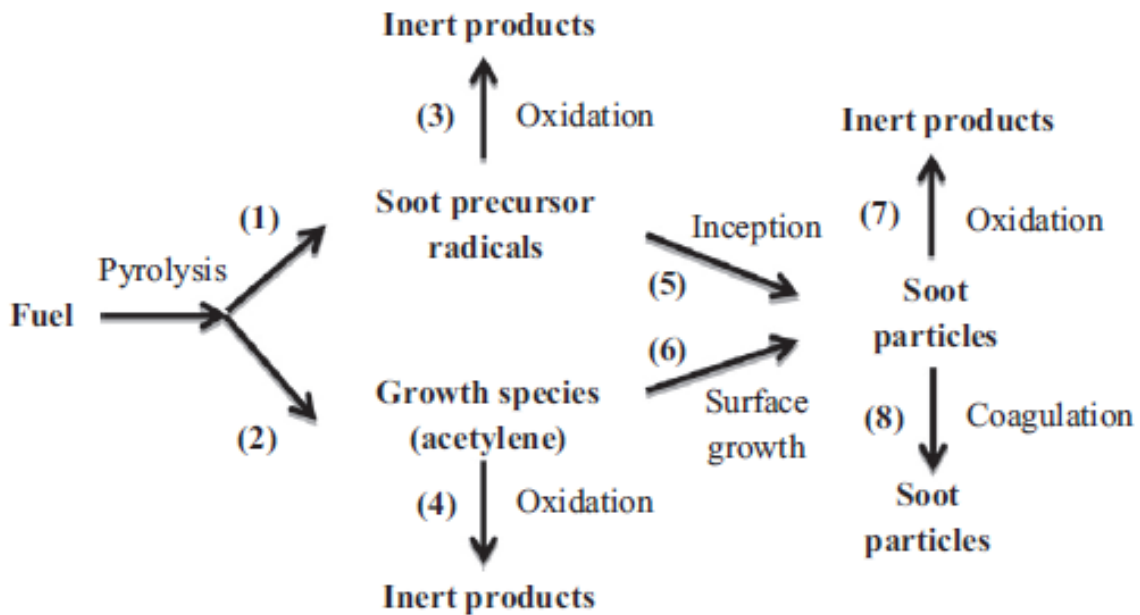


Figure 1: Eight-step sequential diagram of the phenomenological soot model

Eight-step sequential diagram of the phenomenological soot model presented by Fusco et al. [66].

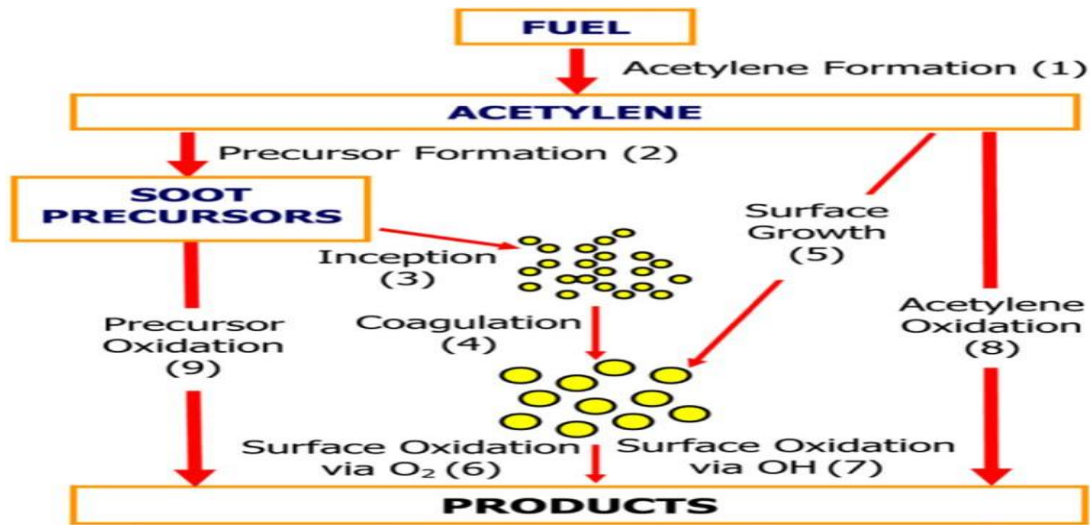


Figure 2: Soot Modeling Mechanism

Soot modeling shown by Tao et al consisting of nine steps [72] mechanisms except for the coagulation and steps of oxidation.

The modeling results incontestable that additional soot is made once more aliphatic compound is offered. The results show that the ultimate quantity of soot is depending on the balance between the formation of soot and oxidization within the each gas and solid phases.

This model contains the important basic procedures concerned in the development of soot throughout combustion procedure; formation of soot precursors, nucleation of the particle of soot, curdling, oxidization and evolution of surface. Once Kazakov and Foster, original model of Fusco's original further explained a nine-step model as conferred below:

1. Soot particle coagulation
2. Formation of acetylene from the fuel pyrolysis
3. Soot precursors role in particle inception.
4. Formation of soot precursor from acetylene.
5. Precursor oxidation by the O_2 .
6. Oxidation by the O_2
7. Surface growth from acetylene.
8. Oxidation by OH.
9. Acetylene oxidation by the O_2 .

The phenomenological model also covers acetylene role in initiation and the growth of surface supposed to be very significant [67] model having nine-step had ultimate weak points that is still

in competent of expressing role of the composition of fuel and the structure although individually of the formation of acetylene rates is reported as it depends on the structure of fuel [25].

In a corresponding study [67], the nine-step phenomenological model of soot was efficient for the prediction of formation of soot and chemical reaction procedures in the diesel engines by Tao et al. [72]. The novel model bestowed by Tao and the coworkers contains 2 components, elaborate chemical action process and the phenomenological semi-empirical model of soot.

Tao's model retained the chief characteristics of the original model [43,66], but it contained three chief variations: (1) Addition of soot oxidation step that is OH-related. In previous study of Liu et al. (2) paralysis of fuel leads solely to the formation of acetylene (3) the precursor of soot is formed simply through acetylene that is not directly from fuel [67]the concentrations of OH were also calculated by the use of the notion of chemical equilibrium.

In the year 2010, Reitz and Vishwanathana [73] has gave the model in its practical form that have foundation non the four essential phases: the inception of soot through the species of PAH that are four-ring, acetylene growth surface, coagulation of the acetylene in forming soot, and oxidation of soot through OH and oxygen. They decided that soot model is justly sensitive to chemical mechanism of PAH[74].

By comparison of experimental results, the necessary enhancements are created in the description model for formation of soot technique under varied environments. The advanced procedures for the formation of soot and oxidization are classified into different steps furthermore as formation of acetylene (C_2H_2)from transformation fuel decomposition, formation of precursor through C_2H_2 conversion, the particle origin from the precursor, and surface growth of particle by C_2H_2 , particle activity, particle surface oxidization through substance oxygen (O_2) and Ohio.

The schematic illustration in Fig. 3 six shows the six-step phenomenological soot model structure that was developed in the study.

- 1.Precursor species that are PAHs (A3, A4) are used.
- 2.In new soot model particle surface growth by A1 is added.

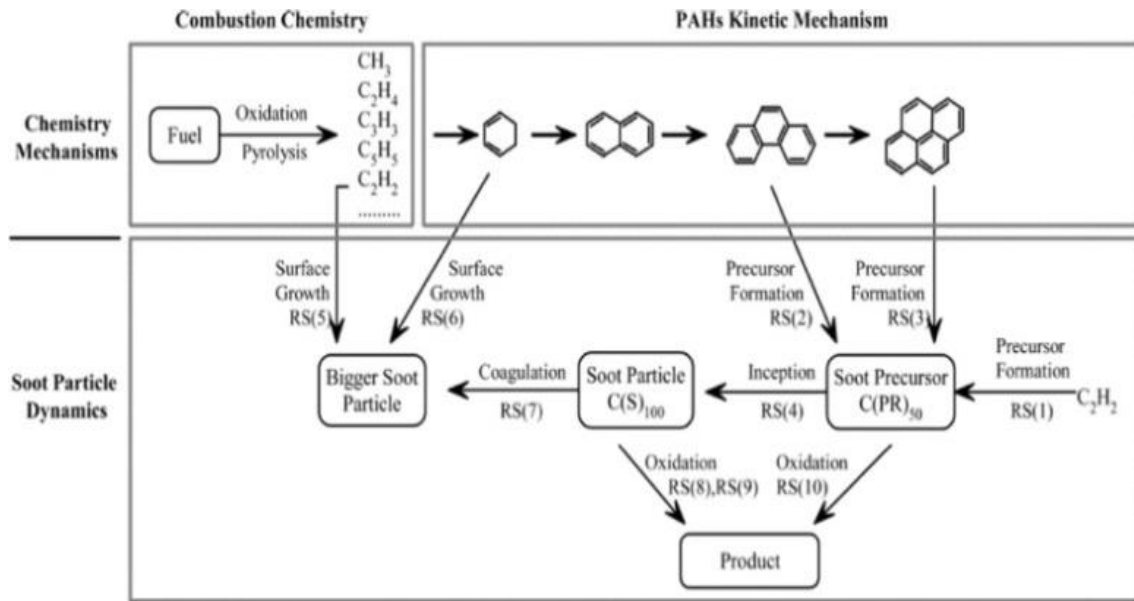


Figure 3: PAHs Kinetic Mechanism

, the atoms of carbons for the precursor of soot and the particle of soot are depicted.

2.2 Objective

In this study, Computational Fluid Dynamics (CFD) based simulation is performed for the catalytic combustion of Methane. In order to incorporate reaction mechanism of the catalytic combustion process, chemkin mechanism file is created which includes the information regarding the chemical reactions involving catalytic combustion of methane and the species that are involved in the process. After the incorporation of required input data to the software, simulation analysis is performed, and results are obtained.

Chapter 3

Modeling

Mechanism of soot is troublesome to be statistically shape due to the massive variety of the primary elements of the diesel oil, quite advanced combustion processes, and also the diverse interactions throughout the formation of soot [41]. Soot models generally classified into 3 more subgroups [42].

Empirical models use links of the experimental information for the prediction of trends in the soot production [43–45]. These models are simple to implement and supply glorious correlations for the given set of in operation situations. Though, the empirical models cannot be wont to examine the underlying mechanisms of the soot production. Consequently, these models don't seem to be such comprehensive to work with variation in the operation conditions. These are solely helpful to examine the antecedently well-known intended experiments underneath precise conditions. Detailed theoretical models use complex mechanism of reactions that consist of many steps so as to expect the concentrations of the soot. Elaborate hypothetical soot models that contained the parts involved in the formation of soot with the high level of the different comprehensive chemical and the physical processes. Such type of inclusive models typically take high money burden for the programming and operational, and far machine time for supplying a converged resolution. On the opposite hand, many empirical and the semi-empirical models overlook a number of many main points so as to create complicated model easy and to cut back the machine price and time. Because of the recent progress in technology in computation, it has become additional possible of using elaborate theoretical models and to acquire more accurate results. Though, more development of the comprehensive theoretical models should be led by more elaborate and correct mechanisms of formation.

3.1 Methodology

3.1.1 Preprocessing The preprocessing consists of the following steps:

Computer-aided design (CAD) can be used to define the physical bound and geometry of the problem. From there, fluid volume is extracted. • The volume which is occupied by the fluid is then divided into discrete cells (mesh

3.1.2 Processing

Simulations are processed until the convergence is reached and the differential equations are solved as steady-state or transient.

3.1.3 Post processing

Finally, the post-processing is done to aid the visualizing and analysis of the solution.

3.2 Simulation Environment

Geometries made in many different software software such as Gambit, Solid Works, Auto CAD, IGES, ANSYS Fluent etc. ANSYS fluent is used to make geometry for simulation of pollutant production.

3.3 Numerical Methodology for 3D Simulation

Setup For three-dimensional modeling, following procedure was adopted for the simulation setup.

- a) Geometry creation
- b) Boundary Conditions
- c) Solver Setting
- d) Post Processing

3.3.1 Geometry creation

3D geometry was constructed for combustion model in the design modular. The dimension of the catalytic combustion model is taken from the previous work.

3.3.2 Meshing

When doing simulations in ANSYS, the solution of the problem depends strongly on the mesh quality. It is very necessary to have a reasonable mesh to solve the problem. The meshing of the computational domain is done in ANSYS Fluent CFD. ANSYS Fluent is a sophisticated tool for mesh creation. 2D Mesh was generated for the combustion chamber. The physical process is done numerically by solving equations of the mathematical model in the computer system. This

representation of equations is usually known as Numerical Simulation. This process has a tendency to produce results that are not achievable through other means. Numerical simulation usage is increasing day by day due to the increase in computer technology. By centralizing a computing capacity in a single system to enhance the performance of that system is regarded as the best way to solve complex problems that can occur in the field of physics and engineering. The evolution in the computer market has made the researcher think to find the new ways of solving complex problems by using computer systems. This can save a lot of time and cost as well. Different simulation tools are available in the market to solve a different set of complex reactions and problems. Computational fluid dynamics is that branch of mechanical science that tends to analyze and solve problems which involve fluid flow systems in chemical reactors. This is way CFD software pack is known as the best designing tool for different areas of reaction engineering as well. This thesis is being done for the numerically simulated combustion process in the presence of a platinum group metal as a catalyst. Two-dimensional (2D) CFD analysis are being done in this research thesis.

Methane combustion is performed under catalytic overheated wall surfaces. Rhodium is used as the catalyst surface for this process of combustion of methane. The chemical reactions which involve catalytic activity taking place on the surface of the catalyst require modeling of a cylindrical channel of heated catalyst wall which is used as a surface phenomenon for the catalytic combustion of methane inside the combustion chamber (Hickman and Schmidt 1993).

For two-dimensional (2D) modeling of the reactor, the cylindrical channel was designed with the 2D axisymmetric solver. The first step of simulation was to create a geometry model which represents the desired flow. Gambit software was used to create the geometry and mesh involving catalyst channel. Two-dimensional CFD code was used for this work. The reactor boundaries such as inlet, outlet and walls wereresolved on this software. The geometry consisted of catalytic walls through which the fuel-air mixture is passed on at high temperature. The inlet temperature of the feed was set 300K, and the wall temperature was set at 2600K. The three important parameters to evaluate the mesh quality are minimum orthogonal quality, maximum Ortho-Skew and maximum aspect ratio. Orthogonal quality ranges from 0 to 1, where values which are closer to 0 corresponds to low mesh quality. Similarly, Ortho Skew ranges from 0 to 1,

where values closer to 1 are considered as the low mesh quality. The mesh generated for 2D had these values as 0.843787, 0.187859 and 5.38952 respectively. Table 1 presents the mesh characteristics such as minimum volume, maximum volume, total volume, no of elements, wedges, minimum face area and maximum face area. The total volume is a summation of volumes of all triangular cells present in geometry. Table

Table 1 Value of Different Mesh Properties

Mesh properties	Values
Orthogonal quality (Minimum)	1.0
Ortho Skew (Maximum)	0.0
Aspect Ratio (Maximum)	109.6
No of Nodes	1705
Quadrilateral cells	1615
Symmetry faces	58
Wall faces(Zone 7)	58
Wall faces(Zone 2)	9
velocity-inlet faces(Zone 8)	20
velocity-inlet faces(Zone 6)	5
Interior faces	3141
Pressure outlet faces	28

A simulation involving diesel combustion process was performed in Fluent 18.0. Species transport model was selected for the process. Wall surface reactions and heat of surface reactions

were selected for the reaction type, and laminar finite-rate was selected for turbulence-chemistry interaction. Boundary conditions for inlet and wall were applied. The fluid regime, type of 32 reactions either volumetric or surface type, kinetic and thermodynamic parameters of reactions, etc. were inserted. All the reactions considered in this work were supposed as the Surface type reactions. Gas mechanism and surface mechanism files were imported into the fluent for the reactions involved in the process. These files had the details of the surface chemistry and surface reactions which contributed to the catalytic combustion

3.3.3 Steps of Creating Mesh

Following steps are performed for the mesh creation: a) Geometry import to ICEM CFD

- b) Blocking of the geometry
- c) Splitting of the Blocks according to the requirement
- d) Blocking associations are done
- e) The setting of the edge parameters
- f) Generating Pre-mesh
- g) Checking quality
- h) Setting output solver

The quality of the mesh created for the present model is above 0.6 which is in accordance with the mesh quality criteria defined by ICEM CFD.

3.4 The NO_x and SO_x model

Large amount carcinogenic pollutants containing Sulphur and nitrogen are emitted in to air by the combustion of the fossil fuels. Seven different types of Oxides of Nitrogen a group term used for family is NO_x and consequently for different oxides of Sulphur is SO_x. On the left-hand aspect, the primary term defines the temporal amendment of the NO concentrations, and therefore the second shows convection amendment. On the right-hand aspect, the primary term defines the distributive amendment, whereas last term is for the supply of NO. Generally, the said atomic number 7 oxides formation procedure along comprise the NO supply term, as seen in combining weight. (11). The thermal mechanism forms atomic number 7 oxides in the post-flame regions by chemical reaction of nitrogen, quick NO is created in reactions of molecular atomic number 7 with organic compound radicals, and therefore the fuel NO happens because

the results of the many corresponding reaction ways from fuel contained atomic number 7. However, in the compression-ignition engine the applications fuel NO is taken into account inapplicable (Mobasheri et al.,

3.5. Effect of turbulent variations

The effect of turbulent variations of the temperature and concentrations of species on production of NO is extremely nonlinear. Their result is taken into consideration by considering chance Density operate (PDF). PDF is supposed to be a two-moment beta operate, as applicable for the combustion calculations.

Formation of soot and reaction are terribly complicated. The extraordinarily increased demand of the calculating time of elaborate models of soot makes them impossible for the simulation of the combustion of ICE. Later, many of the investigations were conducted in an exceedingly real configuration like diesel engines use the procedure of coarse modeling schemes for the requirement of benefit of straightforward application and the low machine value. With the new advances in engineering and the advances indifferent precise sub-models, it is currently attainable to get helpful assumptions and also conceptions of advanced systems. Consequently, the arithmetic simulation of the such advanced systems is taken into account in many fields. In the modeling of soot, many numerical approach of simulations CFD modeling and phenomenological models. In phenomenological models explain the formation of soot and reaction in the terms that is beneficial for the combustion simulations. Soot formation in confined turbulent jet diffusion by using soot particle mass density (M) and variety density (N) was explained by Brookes and Moss [116]. the simulation of the combustion of ICE. Later, many of the investigations were conducted in an exceedingly real configuration like diesel engines use the procedure of coarse modeling schemes for the requirement of benefit of straightforward application and the low machine value. With the new advances in engineering and the advances indifferent precise sub-models, it is currently attainable to get helpful assumptions and also conceptions of advanced systems. Consequently, the arithmetic simulation of the such advanced systems is taken into account in many fields. In the modeling of soot, many numerical approach of simulations CFD modeling and phenomenological models. In phenomenological models explain the formation of soot and reaction in the terms that is beneficial for the combustion simulations. Soot formation in confined turbulent jet diffusion by using soot particle mass density (M) and variety density (N) was explained by Brookes and Moss [116].

$$\frac{DN}{DT} = \left(\frac{dN}{dt}\right)_{Inc.} + \left(\frac{dN}{dt}\right)_{Coa.} \quad (1)$$

$$\frac{DM}{DT} = \left(\frac{dM}{dt}\right)_{Inc.} + \left(\frac{dM}{dt}\right)_{Coa.} + \left(\frac{dM}{dt}\right)_{Oxi.} \quad (2)$$

Whereas there are many models that describe growth, inception, oxidation, and the coagulation terms given in the equations above.

3.6 Soot inception term

Soot origination rate is increased by the presence of aromatic fuels like kerosene as compared to the non-aromatic fuels. During the study the models taken under observation are the two inception models.

There is the detail of models that are used for calculation of soot number density below.

The change in rate of the density of soot mass as compared to number density is given below

$$\frac{dM}{dt} = \frac{M_p}{N_A} \left(\frac{dN}{dt}\right)_{Inc.} \quad (3)$$

Whereas the mass of soot nucleus M_p , has the value of

nearly 1200 kg/kmol (that is based on supposition that size of soot corresponds to the 100 atoms of carbon [115]), and the Avogadro's number that has the value of N_A (6.022045e26/kmol) .

3.6.1 Acetylene inception model

The inception of soot is the first order kinetics of the concentration of the acetylene as described by acetylene inception model [115]. By taking under consideration the following sequence, as the foremost involvement to the inception of soot,



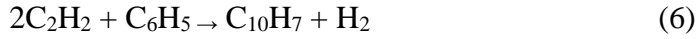
the rate of inception is expressed as,

$$\left(\frac{DN}{Dt}\right)_{Inc.} = c_1 N_A \left(\rho \frac{Y_{C_2H_2}}{W_{C_2H_2}}\right) e^{-\frac{21100}{T}} \quad (5)$$

where the $c_1 = 54 \text{ s}^{-1}$ calculated by the Moss and Brookes [116] and Lindstedt described the temperature of activation [22]

3.5.2 PAH inception model

Formation rate of the two and three aromatic ringed ($C_{10}H_7$ and $C_{14}H_{10}$), from benzene (C_6H_6), the acetylene (C_2H_2), phenyl radical (C_6H_5) is the basis of soot inception rate that is given by Hall *et al.* [113] that is based on following process,



and



The rate of inception of the particle of soot appears to be eight times more than the rate of formation of species $C_{14}H_{10}$ and the $C_{7}H_{10}$ based on the laminar methane flame data of methane that is calculated by Hall *et al.* [113].

$$\left(\frac{DN}{Dt}\right)_{Inc.} = 8 \cdot c_2 \frac{N_A}{M_P} \left[\rho^2 \left(\frac{Y_{C_2H_2}}{W_{C_2H_2}}\right)^2 \frac{Y_{C_6H_5} W_{H_2}}{W_{C_6H_5} Y_{H_2}}\right] e^{-\frac{4378}{T}} + 8 \cdot c_3 \frac{N_A}{M_P} \left[\rho^2 \frac{Y_{C_2H_2} Y_{C_6H_6} Y_{C_6H_5} W_{H_2}}{W_{C_2H_2} W_{C_6H_6} W_{C_6H_5} Y_{H_2}}\right] e^{-\frac{6390}{T}} \quad (8)$$

Where

$$C_2 = 127 \times 10^{8.88} \text{ and } C_3 = 178 \times 10^{9.50}$$

as Hall *et al.* [113] determined.

3.7 Coagulation term for soot

The coagulation of the particles of soot is due to the collisions with one another. Soot is mostly formed of the circular particles that are grouped together to form different shapes and arrangements like chain as given in Fig. 1a. The process of coalescence means the combination of smaller molecules to form huge particle during different processes like growth of particle and nucleation. If it is supposed, like every collision can lead to effective change of the integrity of particles, rate of coagulation is given by

$$\left(\frac{DN}{Dt}\right)_{Coa.} = - \left(\frac{24R}{\rho_{soot} N_A}\right)^{1/2} \left(\frac{6}{\pi \rho_{soot}}\right)^{1/6} T^{1/2} M^{1/6} N^{11/6} \quad (9)$$

where R is a universal gas constant and $\rho_{soot} = 2000 \text{ kg/m}^3$. The inception of soot is the first order kinetics of the concentration of the acetylene as described by acetylene inception model [115]. By taking under consideration the following sequence, as the foremost involvement to the inception of soot.

3.8 Soot growth term

The rate of growth is imperfect because of two reasons; the amount of active sites on surface of soot and the acetylene amount in the flame as the growth rate is primarily calculated by adding acetylene terminated by Frenklach et al. [121] and Harris et al. [122]. The number of active sites are directly related to the surface area of particles. The activation temperature was adjusted at 12,100 K for growth surface during study [115].

$$\left(\frac{DM}{Dt}\right)_{Gro.} = C_4 \left(\rho \frac{Y_{C_2H_2}}{W_{C_2H_2}}\right) e^{-\frac{12100}{T}} [(\pi N)^{1/3} \left(\frac{6M}{\rho_{soot}}\right)^{2/3}] \quad (10)$$

where $C_4 = 9000.6 \text{ kg} \cdot \text{m} \cdot \text{kmol}^{-1} \cdot \text{s}^{-1}$.

3.9 Term of soot oxidation

The process of oxidation takes place all the time in precise stage in contrast to growth of soot surface, O_2 and OH radical are most leading species in the soot oxidation. Neoh et al. [17] considered OH radical as the primary oxidant and by the kinetic theory studied about the consumption of the soot mass. Removal of single atom of carbon from the molecule of soot that is the fraction of collision is referred as colliding potency parameter. The rate of oxidation is affected by the area of particles. The averaged value calculated in their flames is 0.13 and is dependent on size of a primary particle used in the research.

By assuming the particles small so that diffusion rate on oxidation of soot by oxygen can be ignored and surface reaction kinetics the limiting method Lee et al. [19] and find out how soot oxidation depends upon stoichiometric amount of O_2 during diffusion of laminar flame during his research work equation by Lee was transformed in terms of SI units and make it applicable to current soot model. Now, mathematically rate of soot oxidation is given as

$$\left(\frac{DM}{Dt}\right)_{Oxi} = -c_5 \eta \rho \frac{Y_{OH}}{W_{OH}} \sqrt{T} (\pi N)^{1/3} \left(\frac{6M}{\rho_{soot}}\right)^{2/3} - c_6 \rho \frac{Y_{O_2}}{W_{O_2}} \exp\left(-\frac{19778}{T}\right) \sqrt{T} (\pi N)^{1/3} \left(\frac{6M}{\rho_{soot}}\right)^{2/3} \quad (11)$$

where η is set to be 0.13, $c_5 = 105.81 \text{ kg} \cdot \text{m} \cdot \text{kmol}^{-1} \cdot \text{K}^{-1/2} \cdot \text{s}^{-1}$, that is obtained by converting the soot consumption mass rate, calculated by Neoh et al. [17], into System International units, $c_6 = 8903.51 \text{ kg} \cdot \text{m} \cdot \text{kmol}^{-1} \cdot \text{K}^{-1/2} \cdot \text{s}^{-1}$ [18].

3.10 Transport equations for soot

The important supposition made during the study was that levels of chemical species is not effected by the soot formation. On the flame the soot was treated as perturbation due to small volume. This will be probable to overvalue the levels of soot as using up of species is unnoticed. The oxidation and formation rates of soot are the complex functions of the species consumption, temperature, density, the temperature as shown in the Equations 5 and Equations 8–11.

The conservation equation described by any of the dependent scalar variable if the constraints of the soot, *i.e.* mass density (M), the number density of soot particle (N) will be expressed as,

$$\frac{\partial}{\partial t}(\rho\phi) + \frac{\partial}{\partial x_j}(\rho u_j \phi) = \frac{\partial}{\partial x_j} \left(D \frac{\partial \phi}{\partial x_j} \right) + S_\phi \quad (12)$$

The four terms in the Eq. 12 represents the transient, the convective, the diffusive, also the source terms, correspondingly. Source term, S_ϕ , is calculated by the model of soot.

For the numerical ease, two variables the M and N are given by

$$N = N_A \rho \phi_N \quad (13)$$

$$M = \rho \phi_M \quad (14)$$

Therefore, source terms for the ϕ_N and ϕ_M can also be described as,

$$S\phi_N = \frac{d(\rho\phi_N)}{dt} = \frac{1dN}{N_A dt} \quad (15)$$

$$S\phi_M = \frac{d(\rho\phi_M)}{dt} = \frac{dM}{dt} \quad (16)$$

Right sides of these equation coressponds to eq.1 and eq.2

3.10 Term of source linearization

In CFD solver for linearization of source terms Newton-Raphson [23]. Using this scheme, source term can be expressed as,

$$S\phi = S\phi^0 + \left(\frac{dS\phi}{d\phi}\right)^0 (\phi - \phi^0) = \left\{ S\phi^0 - \frac{dS\phi}{d\phi} \Big|_0 \phi^0 \right\} + \frac{dS\phi}{d\phi} \Big|_0 \phi. \quad (17)$$

It is significant that active term,

$\frac{dS\phi}{d\phi} \Big|_0$ be negative, or else the time rate of convergence is also compromised.

CHAPTER NO 4

Results and Discussions

Result and Discussions

The structure of flame during non-laminar flow field gives input to the soot model. As a result, accuracy of soot model depends upon good interaction of turbulent flow variables with measurements obtained from experiments. In this part, the contours of numerous important physical parameters in the non-laminar combustion field are presented first. Finally, the results from simulation are compared with experimental data.

Table.2 Results of simulation and experimental data are given below

Parameters	Inlet Fuel	Inlet Air
T(K)	598	300
k (m ² -s ⁻²)	0.03	0.03
Velocity	22.3	0.234
ε (m ² -s ⁻³)	0.02	0.02
Wall		T=300K
Outlet		P=1 barr

Temperature Profile [K]is shown below

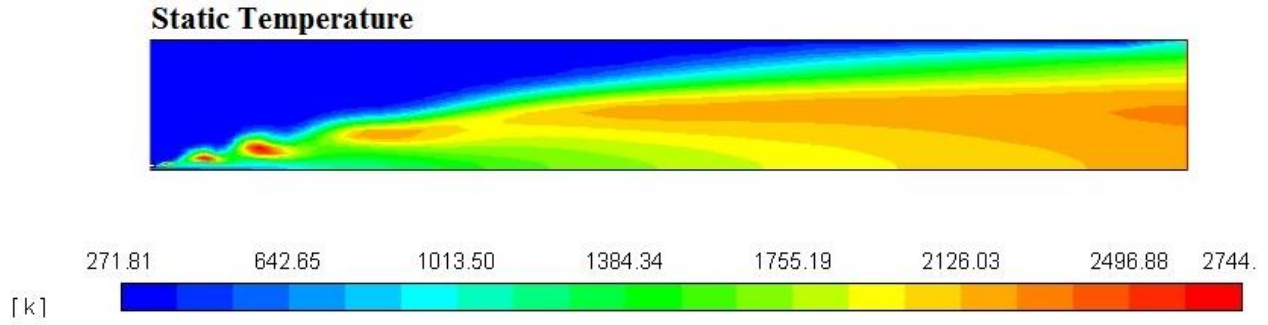


Figure 4: Temperature Profile

Specific Heat Profile/Cp [J/Kg-K] diagram is given below

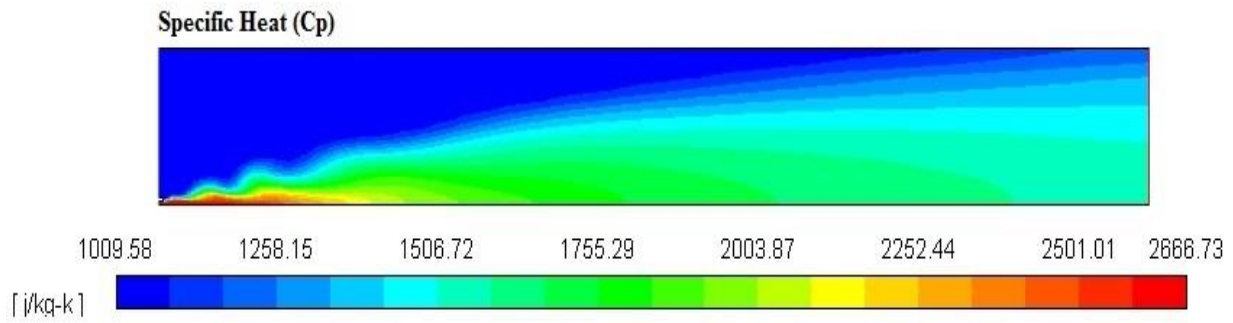


Figure 5: Specific Heat Profile

Velocity Magnitude Profile [m/s] is expressed below

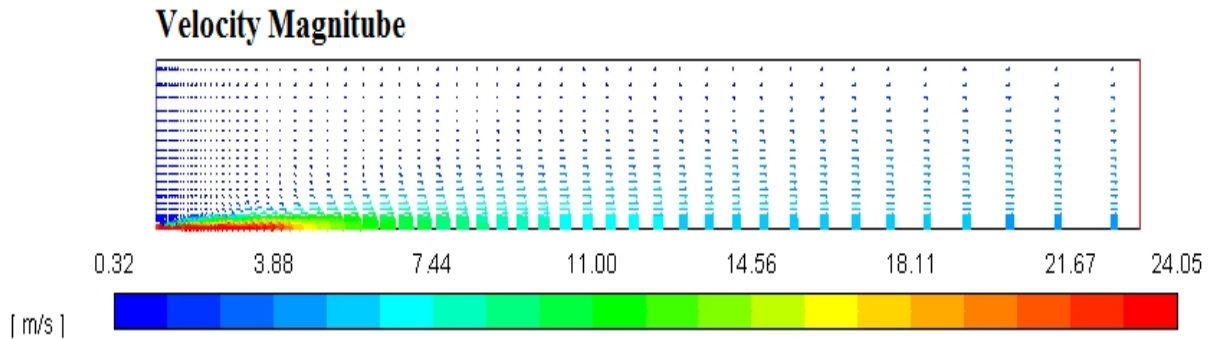


Figure 6: Velocity Magnitude Profile

Stream Function Profile [Kg/s] is shown in the figure below

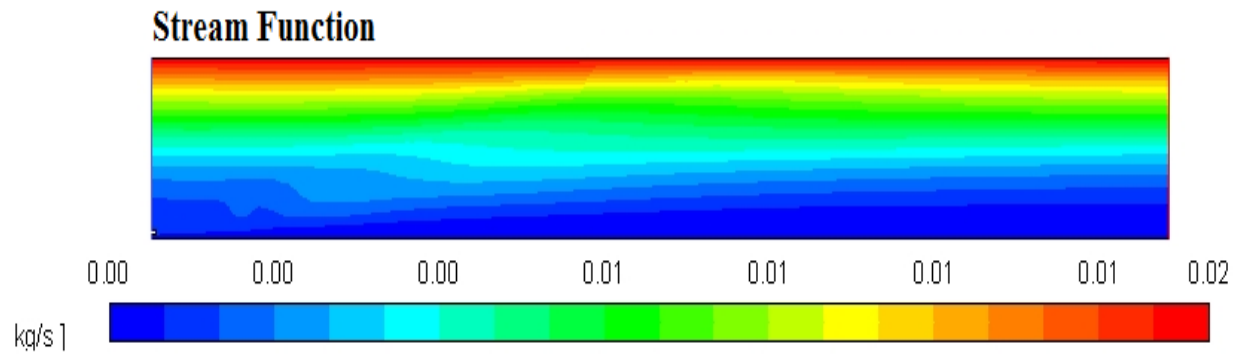


Figure 7: Stream Function Profile

Diesel Mass Fraction Profile is given as

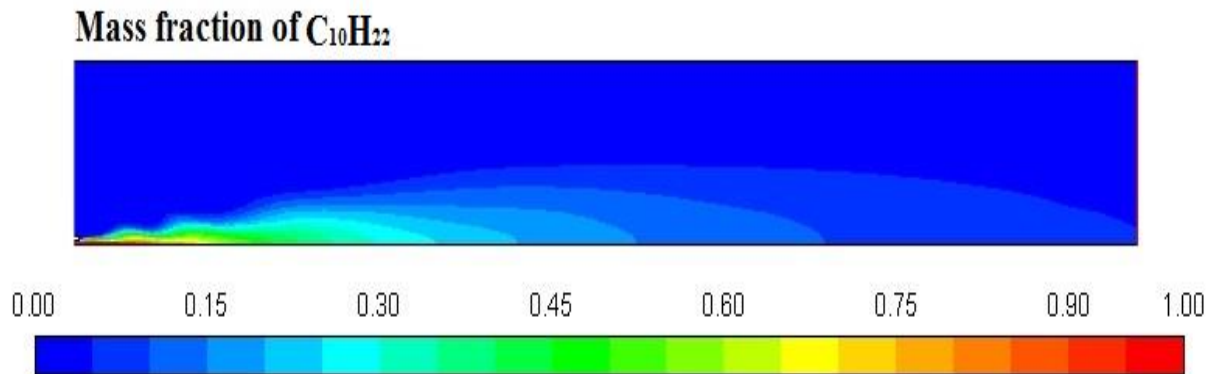


Figure 8: Diesel Mass Fraction Profile

O₂ Mass Fraction Profile is shown in the figure

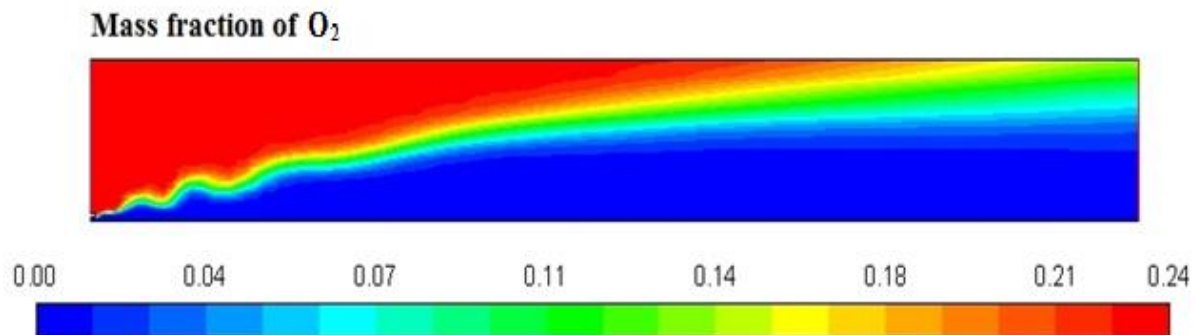


Figure 9: O₂ Mass Fraction Profile

CO₂ Mass Fraction Profile is expressed below

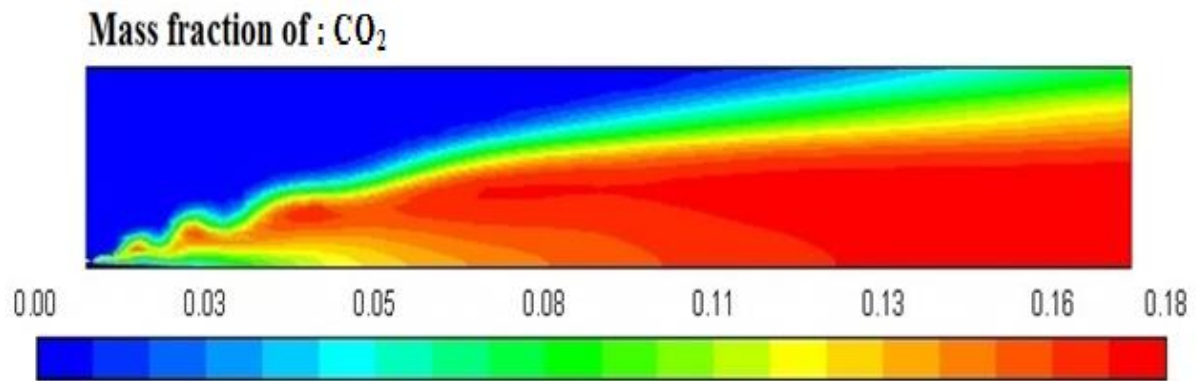


Figure 10: CO₂ Mass Fraction Profile

H₂O Mass Fraction Profile is given in the figure below:

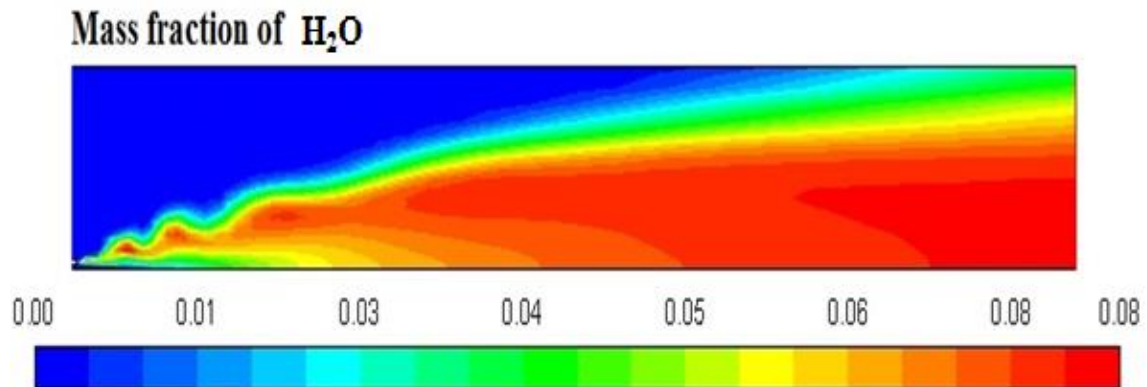


Figure 11: H₂O Mass Fraction Profile

Soot Mass Fraction Profile is expressed below

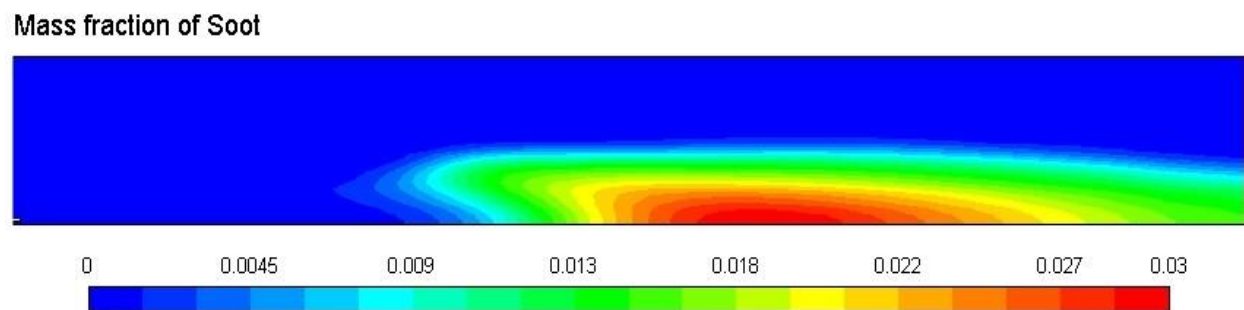


Figure 12: Soot Mass Fraction Profile

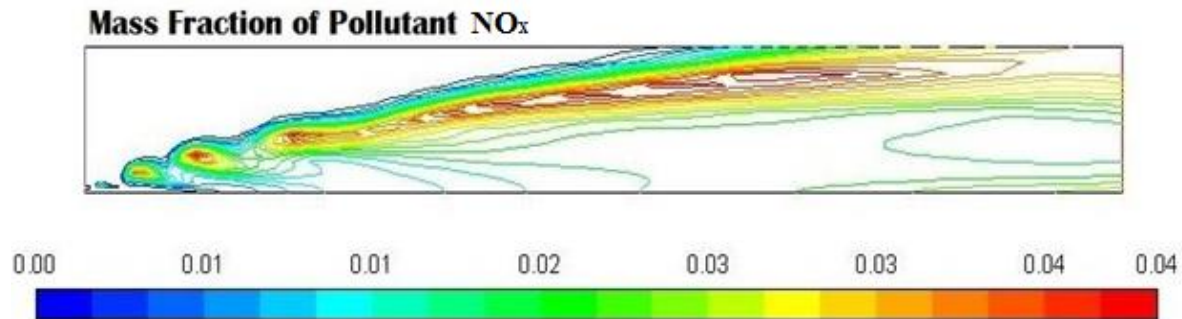


Figure 13: Mass Fraction of Pollutant NO_x

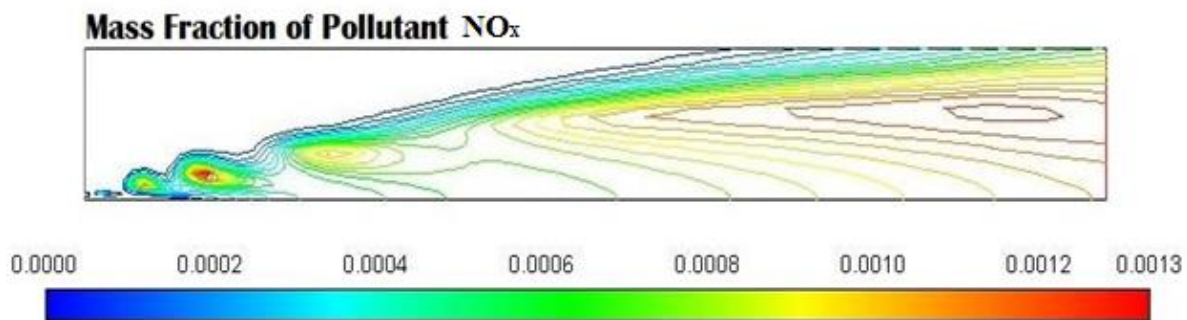


Figure 14: Mass Fraction of NO_x without prompt Nox mechanism

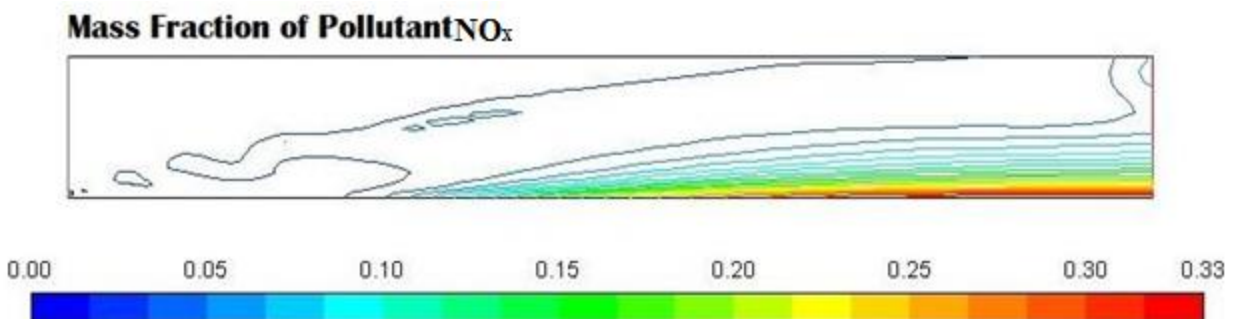


Figure 15: Mass Fraction of NO_x with only prompt NO_x Mechanism NO_x

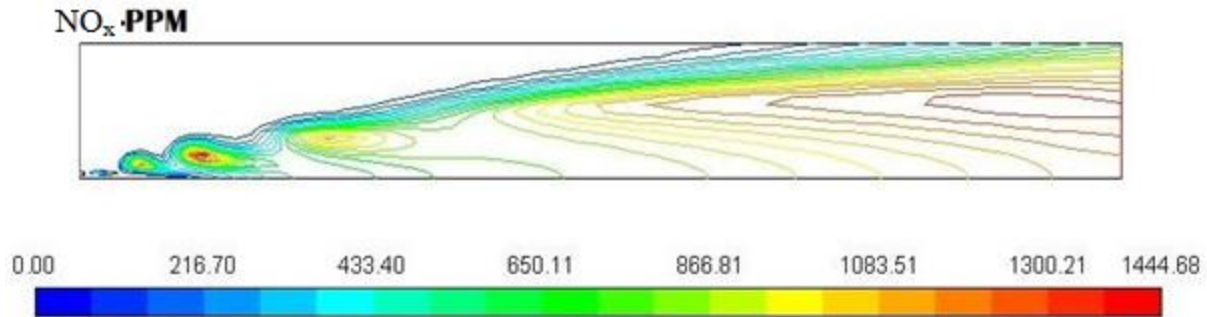


Figure 16: Concentration of NO_x in terms PPM

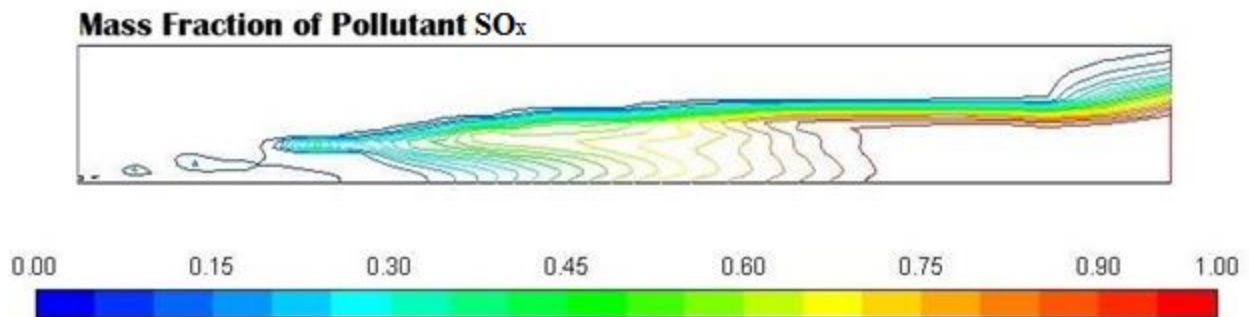


Figure 17: Mass Fraction of pollutant SO_x

Figure 4 , the peak temperature, predicted using a constant heat capacity of 1000 J/Kg K, is about 2744 K from 300 K. The temperature is increased due high pressure during compression stroke, over prediction of the same temperature can be reduced by more reality based accurate model for the temperature and composition dependence of the heat capacity.

Figure 5 represents the Cp profile of the combustion chamber, the mixture specific heat is largest where the C₁₀H₂₂ is concentrated, close to nozzle of fuel inlet,

In which zone combustion product concentrations and temperature is increased. The increase in heat capacity to 2644 J/Kg. K, relative to the constant value used before, substantially lowers the peak flame temperature.

Figure 6 represents the velocity profile of the combustion chamber. In the annulus region, velocity increases sharply from around 0.3 m/sec to 24 m/sec due to a decrease in the cross-sectional area while entering in nozzle combustion chamber through inlet nozzle to provide sufficient Kinetic energy to increase temperature and pressure for ignition stroke.

Figure 7 represents the profile of stream function whose value is increased up to 0.02 that clearly represents entrainment of air into the high-velocity Diesel jet is clearly visible in the streamline display.

Figures 8,9,10,11 represent the variation in mass fraction of diesel, Oxygen, CO₂ and H₂O respectively. Conversion Diesel takes place through combustion so its mass fraction reduced to zero. Similarly the mass fraction of oxygen is also reduced to almost zero from 0.24. On the other hand, CO₂ is formed BY combustion reaction so its mass fraction increases up to 0.24 as water is also formed in combustion so mass fraction H₂O is also observed upto 0.08 and small amount of soot is also observed as a result of combustion reaction during diesel combustion.

Figure.12 show the soot formation during the combustion of diesel in turbulent diffusion flame furnaces and soot amount predicted through the Moss Brooks model is 0.03 that is approximately equal to the experimental value.

Figure.13 explain the NO_x formation during combustion of diesel in engines, model predict NO_x formation in a "post processing" mode, with the temperature, and hydrocarbon combustion species concentrations. Thus, only the NO equation will be computed. Prediction of NO in this mode is justified on the grounds that the NO concentrations are very low and have negligible impact on the Diesel combustion prediction.

Figure.14 explains the prediction without the prompt NO_x mechanism and the concentration of NO is slightly lower without the prompt NO_x mechanism.

Figure.15 explain the prediction with the prompt NO_x mechanism only and the concentration of NO is more increased with the prompt NO_x mechanism and it is noted that individual thermal and prompt NO mass fractions do not add up to the Levels predicted with the two models combined. This is because reversible reactions are involved. NO produced in one reaction can be destroyed in another reaction.

Figure.16 contours closely resemble the mass fraction contours (Figure 12), as expected its represents the total concentration of NO_x in terms of ppm and nearly equal value to experiment calculated results.

Explain the SO₂ formation during combustion of diesel in engines, model predict SO₂ with the temperature, and hydrocarbon combustion species concentrations . SO₂ prediction in this mode is justified on the grounds that the NO concentrations are very low and have negligible impact on the Diesel combustion prediction.

Comparison of results with experimental/Literature data

Functions	Literature Data	Model results	Variation
Peak Temperature	2150	2200	2%
Soot volume Fraction	2.7e-06	3.5e-06	18%
Soot Mass Density	4.0e-03	6.13-03	33%

Results compared with Z. Wen et al. / Combustion and Flame 135 (2003) 323–340 325 [112].

Figure.18 comparison of soot volume fraction of model and literature

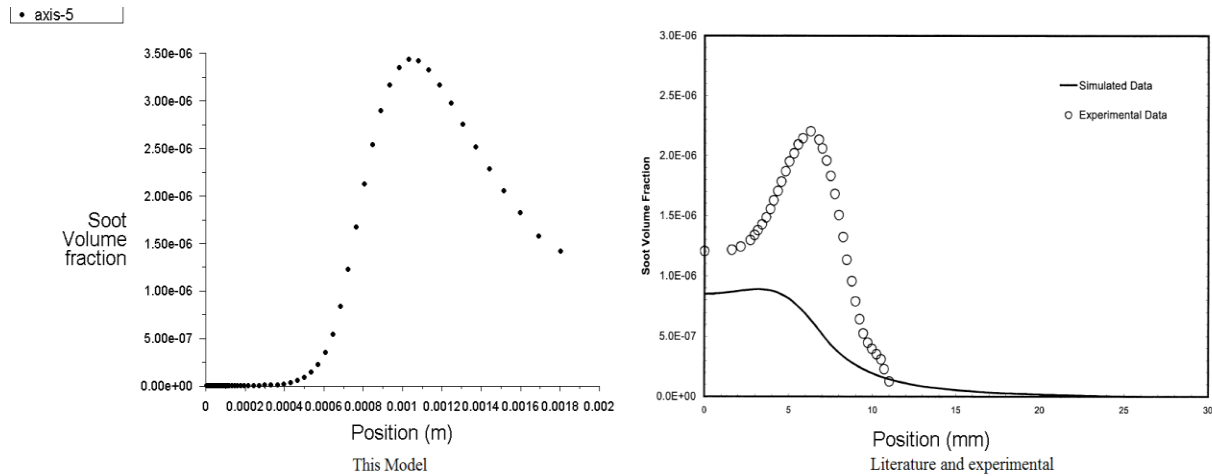


Figure 18: comparison of soot volume fraction

Comparison of peak temperature profile of model and literature

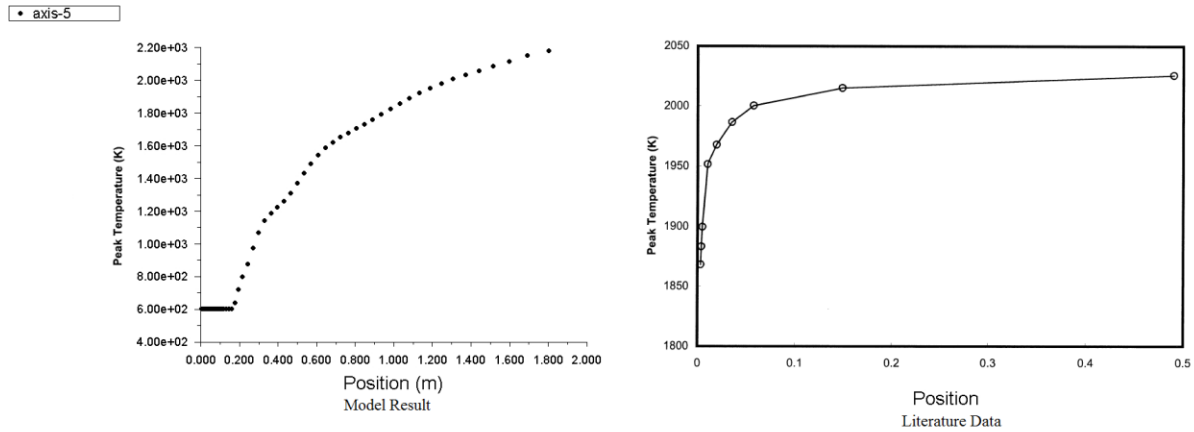


Figure 19: Comparison of peak temperature profile

A two-dimensional combustion model for riser has been developed by using commercial CFD code FLUENT 18.0 with the assistance of model. It is observed that the model prediction for soot has increase and the rise in temperature of combustion chamber. The model predictions of the soot mass fraction confirmed by evaluation with plant data supplied by Young et al. [114]. A fine agreement was there between model predictions and the experimental data when the more validation was done by comparing the results with numerical work of Wen et al. [112] were considered. Mass fraction contours, riser temperature profiles are predicted by using the Moss Brooks model. The simulation predicts that the exit temperature and exit velocity as well as mass fraction of species along soot. This study was compared with experimental and literature result of Wen et al [112] by peak temperature and soot volume fraction produced during combustion

Conclusions

A two-dimensional and three-dimensional cylindrical reactor has been made by using Ansys Fluent comprising combustion channel inside it for the diesel combustion. Ansys Fluent has been used to predict the behavior of the fluid regimes involving in the process of catalytic combustion. Incorporation of reaction mechanism for the catalytic combustion of methane in the software is done by creating a reaction mechanism file which consisted all the reactions involved in the methane combustion mechanism. The reaction file was imported into the software to conclude reaction mechanism. The simulation was performed on input data, and it is concluded that the mass fraction of reactants decreased as the reaction proceeded through the catalytic channel of the combustion chamber. As a result, increase in product formation is observed. It was noticed that the presence of catalytic channel inside the combustion chamber ignited the combustion reaction. The catalytic activity was the reason to raise the temperature of the combustion chamber. Mass fraction profiles of the reactants and the products of combustion reaction are predicted in this study. This study recommended that the CFD simulation is the best software to predict the behavior of chemical process mainly catalytic combustion. It is concluded through this research that CFD is the best software available for the prediction of surface reaction and related processes.

Future Recommendations

Future work should majorly focus on the following topics for the optimum prediction of fluid regimes of the combustion process and its behavior inside the combustion chamber involving inorganic pollutants and other hydrocarbons.

- Numerical Simulation analysis of the 3D combustion process.
- Optimization of internal combustion engines through simulation using Computational Fluid Dynamics.
- CFD modeling and simulation design for simultaneous removal of volatile organic compounds and sulfur and NO_x particles generated during the combustion process.

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